Excess Molar Volumes and Refractive Indexes of Heptanol + **Pentane,** + **Hexane,** + **Heptane,** + **Octane, and** + **2,2,4-Trimethylpentane**

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Excess molar volumes, $V_{\rm m}^{\rm E}$, have been measured using a direct dilatometric technique for binary mixtures of heptanol (n-C₇H₁₅OH) + hexane (n-C₆H₁₄), + heptane (n-C₇H₁₆), + octane (n-C₈H₁₈), and + 2,2,4-trimethylpentane (2,2,4-TMP) at 308.15 K and for n-C₇H₁₅OH + pentane (n-C₅H₁₂) at 298.15 K. The refractive indexes, $n_{\rm D}$, have been measured for these mixtures at 303.15 K. $V_{\rm m}^{\rm E}$ has been found to be negative throughout the entire range of composition for xn-C₇H₁₅OH + (1 - x)n-C₅H₁₂ and xn-C₇H₁₅OH + (1 - x)n-C₆H₁₄. $V_{\rm m}^{\rm E}$ has been found to be positive at lower values of x and negative at higher values of x for xn-C₇H₁₅OH + (1 - x)2,2,4-TMP, xn-C₇H₁₅OH + (1 - x)n-C₇H₁₅OH + (1 - x)n-C₈H₁₈, with the inversion of sign from positive to negative values of $V_{\rm m}^{\rm E}$ occurring at $x \sim 0.06$, $x \sim 0.20$, and $x \sim 0.45$ respectively for these mixtures. Values of $V_{\rm m}^{\rm E}$ and $n_{\rm D}$ for the various mixtures of n-C₇H₁₅OH have been fitted in smoothing equations.

Introduction

Binary (an alkanol + an alkane) mixtures are of considerable interest from the theoretical viewpoint of the models of the hydrogen-bonded systems. Systematic studies of the thermodynamic excess properties provide important information concerning the deeper understanding of the molecular liquid structure and the intermolecular interactions predominated by the self-association of the alkanol molecules due to hydrogen bond formation. These studies are also important from the viewpoint of the prediction of thermodynamic properties of (alkanol + alkane) mixtures of components having varying numbers of -CH₂- units in the alkyl chain or varying numbers of -CH₃ substituents attached to the alkyl chain in the alkanol or alkane. With this viewpoint, Wagner and Heintz (1986) and Heintz et al. (1986) measured excess molar volumes, $V_{\rm m}^{\rm E}$, of binary mixtures of nonane and hexane with five different 1alkanols at various temperatures. Fuente et al. (1992) determined $V_{\rm m}^{\rm E}$ of (nonan-1-ol + decane or tetradecane) at the temperatures 298.15 K, 308.15 K, and 318.15 K. Franjo et al. (1994) have measured V_m^E of $xCH_3(CH_2)_5OH + (1 - x)CH_3(CH_2)_4CH_3$ at 298.15 K. Zielkiewicz (1994a,b) has measured total vapor pressures and V^{E}_{m} of (heptane + propan-2-ol or butan-1-ol or 2-methylpropan-1-ol or 2methylpropan-2-ol or pentan-1-ol) at 313.15 K. Although Nath and Pandey (1997) have recently made measurements of $V_{\rm m}^{\rm E}$ and refractive indexes, $n_{\rm D}$, for binary mixtures of butanol with pentane $(n-C_5H_{12})$, hexane $(n-C_6H_{14})$, heptane (n-C₇H₁₆), octane (n-C₈H₁₈), and 2,2,4-trimethylpentane (2,2,4-TMP), a systematic study of mixtures of these alkanes with an alkanol of more complexity has not been made. Hence, in this program, measurements of $V_{\rm m}^{\rm E}$ and $n_{\rm D}$ of heptanol (*n*-C₇H₁₅OH) + *n*-C₅H₁₂, + *n*-C₆H₁₄, $+ n-C_7H_{16}$, $+ n-C_8H_{18}$, and + 2,2,4-TMP have been made, and the results of these measurements are reported and discussed in this paper.

Experimental Section

Materials. Pentane, hexane, heptane, 2,2,4-trimethylpentane, all of HPLC quality and stated purity of the order

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of 99.8%, and heptanol, of LR quality and stated purity of 99% (GLC), were obtained from S. D. Fine Chemicals Pvt. Ltd., Mumbai, India. Pentane, hexane, heptane, and 2,2,4-TMP were used without any further purification. Heptanol was dried over anhydrous potassium carbonate and then subjected to distillation, and the middle third cut was used for the measurements. Octane (Spectrochem product) of AR quality and stated minimum purity of 99.5% (GLC) was distilled fractionally before use.

Methods. (i) Excess molar volumes, $V_{\rm m}^{\rm E}$, were measured with an imprecision of the order of $\pm 0.002 \, {\rm cm}^3 \cdot {\rm mol}^{-1}$, using a two-limbed Pyrex glass dilatometer which was similar to that used in earlier measurements (Nath and Saini, 1989; Nath and Chaudhary, 1992; Nath and Pandey, 1997). Known amounts of the two liquid components were confined over mercury in the absence of air spaces in the two limbs of the dilatometer. The dilatometer (mounted on a stand) was immersed in a thermostat which was controlled to ± 0.01 K. The mixing of the two liquid components was done by rocking the cell back and forth through a definite angle, and the mercury levels in the capillary of the dilatometer were noted before and after mixing, using a cathetometer which had the accuracy of ± 0.001 cm, as described earlier (Nath and Pandey, 1997).

(ii) The refractive indexes (sodium D line), n_D , of the pure samples and the various liquid mixtures were measured with an accuracy of ± 0.0002 at (303.15 \pm 0.01) K, using a thermostated Abbe refractometer. The mole fractions of the components in the various mixtures are accurate to ± 0.0001 .

Results and Discussion

The present experimental values of n_D of n-C₅H₁₂, n-C₆H₁₄, n-C₇H₁₆, n-C₈H₁₈, 2,2,4-TMP, and n-C₇H₁₅OH are 1.3520, 1.3695, 1.3825, 1.3925, 1.3865, and 1.4202, respectively. The values of n_D of n-C₅H₁₂, n-C₆H₁₄, n-C₇H₁₆, n-C₈H₁₈, and 2,2,4-TMP at T= 303.15 K, listed in Riddick and Bunger (1970) are 1.352 07, 1.369 55, 1.382 57, 1.392 64, and 1.386 60, respectively. The experimental values of V_m^E for the mixtures of n-C₇H₁₅OH + n-C₅H₁₂, + n-C₆H₁₄,

Table 1. Experimental Values of the Excess Molar Volumes, V_m^E , for $n-C_7H_{15}OH + n-C_6H_{14}$, $+ n-C_7H_{16}$, $+ n-C_8H_{18}$, + 2,2,4-TMP at 308.15 K and for $n-C_7H_{15}OH + n-C_5H_{12}$ at 298.15 K

X	$V_{\rm m}^{\rm E}/{ m cm}^3\cdot{ m mol}^{-1}$	X	$V_{\rm m}^{\rm E}/{ m cm}^3\cdot{ m mol}^{-1}$	X	$V_{\rm m}^{\rm E}/{ m cm}^3\cdot{ m mol}^{-1}$	X	$V_{\rm m}^{\rm E}/{ m cm}^3\cdot{ m mol}^{-1}$				
$xn-C_7H_{15}OH + (1 - x)n-C_5H_{12}$											
0.0248	-0.077	0.2090	-0.439	0.5042	-0.620	0.7713	-0.493				
0.0693	-0.190	0.2705	-0.508	0.6017	-0.614	0.8338	-0.412				
0.1213	-0.303	0.3588	-0.574	0.6381	-0.602	0.8882	-0.303				
0.1550	-0.359	0.3967	-0.595	0.7296	-0.540						
$xn-C_7H_{15}OH + (1-x)n-C_6H_{14}$											
0.0369	-0.013	0.2047	-0.181	0.5173	-0.368	0.8427	-0.230				
0.0843	-0.052	0.2945	-0.261	0.6417	-0.363	0.8710	-0.198				
0.1134	-0.084	0.3722	-0.316	0.6956	-0.343	0.9306	-0.115				
0.1667	-0.143	0.4148	-0.338	0.7203	-0.331						
0.1882	-0.166	0.4655	-0.361	0.8136	-0.257						
	$xn-C_7H_{15}OH + (1 - x)n-C_7H_{16}$										
0.0225	0.042	0.2895	-0.049	0.5634	-0.183	0.8026	-0.168				
0.1153	0.048	0.3323	-0.076	0.5891	-0.195	0.8325	-0.148				
0.1283	0.036	0.3825	-0.100	0.6379	-0.200	0.8545	-0.136				
0.1629	0.020	0.4323	-0.131	0.6879	-0.196	0.8886	-0.117				
0.2276	-0.016	0.4837	-0.154	0.7350	-0.190	0.9400	-0.063				
	$xn-C_7H_{15}OH + (1 - x)n-C_8H_{18}$										
0.0411	0.043	0.1833	0.108	0.4637	-0.012	0.7984	-0.098				
0.0698	0.073	0.2310	0.095	0.4899	-0.028	0.8244	-0.091				
0.0720	0.072	0.2849	0.077	0.5882	-0.072	0.8288	-0.090				
0.1275	0.103	0.3750	0.034	0.6679	-0.099	0.8775	-0.070				
0.1303	0.104	0.4343	0.006	0.7385	-0.103	0.9391	-0.035				
$xn-C_7H_{15}OH + (1 - x)2.2.4$ -TMP											
0.0255	0.025	0.3512	-0.273	0.6713	-0.348	0.9112	-0.149				
0.0419	0.017	0.3806	-0.294	0.7590	-0.306	0.9439	-0.105				
0.1202	-0.052	0.4440	-0.323	0.7958	-0.286	0.9605	-0.073				
0.1851	-0.121	0.5059	-0.347	0.8217	-0.256						
0.2700	-0.207	0.5791	-0.360	0.8777	-0.199						

Table 2. Experimental Values of the Refractive Indexes, n_D , for n-C₇H₁₅OH + n-C₅H₁₂, + n-C₆H₁₄, + n-C₇H₁₆, + n-C₈H₁₈, and + 2,2,4-TMP at 303.15 K

X	n _D	X	n _D	X	n _D	X	n _D		
$xn-C_7H_{15}OH + (1-x)n-C_5H_{12}$									
0.0257	1.3535	0.3003	1.3728	0.5686	1.3910	0.8345	1.4090		
0.1311	1.3610	0.3511	1.3762	0.5836	1.3915	0.8828	1.4120		
0.1429	1.3620	0.4156	1.3805	0.6490	1.3965	0.9442	1.4165		
0.2810	1.3710	0.4314	1.3818	0.7313	1.4015	0.9776	1.4190		
$xn-C_7H_{15}OH + (1 - x)n-C_6H_{14}$									
0.0204	1.3705	0.2852	1.3835	0.5414	1.3972	0.8810	1.4145		
0.1107	1.3748	0.3322	1.3862	0.5859	1.3995	0.9321	1.4168		
0.1364	1.3765	0.3973	1.3898	0.6189	1.4008	0.9665	1.4182		
0.2186	1.3802	0.4276	1.3910	0.6939	1.4045				
0.2466	1.3822	0.5017	1.3950	0.7302	1.4068				
		xn-C7H	$H_{15}OH +$	(1 - x)n	$-C_7H_{16}$				
0.0198	1.3830	0.3040	1.3940	0.5547	1.4032	0.8104	1.4132		
0.0949	1.3858	0.3308	1.3950	0.6109	1.4055	0.8235	1.4135		
0.1339	1.3875	0.4022	1.3980	0.6457	1.4072	0.9216	1.4170		
0.1728	1.3890	0.4493	1.3995	0.7117	1.4095	0.9701	1.4192		
0.2509	1.3915	0.4797	1.4008	0.7482	1.4110				
		xn-C7H	$H_{15}OH +$	(1 - x)n	$-C_8H_{18}$				
0.0365	1.3935	0.4359	1.4045	0.6842	1.4115	0.8581	1.4160		
0.1560	1.3965	0.4505	1.4048	0.6918	1.4115	0.9386	1.4182		
0.2789	1.4000	0.5374	1.4070	0.7547	1.4135				
0.4070	1.4035	0.6000	1.4088	0.7950	1.4148				
xn-C ₇ H ₁₅ OH + (1 - x)2,2,4-TMP									
0.0331	1.3875	0.3256	1.3975	0.5914	1.4062	0.8277	1.4145		
0.1280	1.3908	0.3527	1.3985	0.6269	1.4075	0.8947	1.4165		
0.1693	1.3925	0.4308	1.4012	0.6717	1.4090	0.9296	1.4178		
0.1960	1.3932	0.4922	1.4030	0.7424	1.4115	0.9479	1.4185		
0.2694	1.3955	0.5115	1.4040	0.7903	1.4130				

+ n-C₇H₁₆, + n-C₈H₁₈, and + 2,2,4-TMP are given in Table 1, whereas the values of n_D for these mixtures at 303.15 K are given in Table 2, where *x* refers to the mole fraction of n-C₇H₁₅OH in the mixture. *x* has an uncertainty of ± 0.0001 . Values of V_m^E for the present mixtures have been plotted against *x* in Figure 1 and have been fitted by the method of least squares to the equation



Figure 1. $V_{\rm m}^{\rm E}$ plotted against *x* for the following systems: (\Box) *xn*-C₇H₁₅OH + (1 - *x*)*n*-C₅H₁₂, *T* = 298.15 K; (\triangle) *xn*-C₇H₁₅OH + (1 - *x*)*n*-C₆H₁₄, *T* = 308.15 K; (\odot) *xn*-C₇H₁₅OH + (1 - *x*)*n*-C₇H₁₆, *T* = 308.15 K; (\blacksquare) *xn*-C₇H₁₅OH + (1 - *x*)*n*-C₈H₁₈, *T* = 308.15 K; (\blacksquare) *xn*-C₇H₁₅OH + (1 - *x*)2,2,4-TMP, *T* = 308.15 K.

$$V_{\rm m}^{\rm E}/x(1-x) = \sum_{j=1}^{m} A_j Y_j$$
(1)

where $Y_j = [x - 1/(1 + Dx)]^{j-1}$ and A_j are the coefficients characteristic of a system at a given temperature. As

Table 3. Values of the Coefficients A_i of Eq 1 and the Standard Deviations, $\delta(V_m^E)$, for the Various Mixtures

			cm³∙mol ^{−1}				
mixture	<i>T</i> /K	A_1	A_2	A_3	A_4	$\delta(V_{\rm m}^{\rm E})$	
xn-C ₇ H ₁₅ OH + (1 - x) n -C ₅ H ₁₂ xn-C ₇ H ₁₅ OH + (1 - x) n -C ₆ H ₁₄ xn-C ₇ H ₁₅ OH + (1 - x) n -C ₇ H ₁₆ xn-C ₇ H ₁₅ OH + (1 - x) n -C ₈ H ₁₈ xn-C ₇ H ₁₅ OH + (1 - x)2.2.4-TMP	298.15 308.15 308.15 308.15 308.15	-2.6871 -1.0462 0.0962 0.7271 -0.7922	$\begin{array}{r} 0.9160 \\ -1.2040 \\ -2.1882 \\ -1.8080 \\ -1.8824 \end{array}$	$-0.5902 \\ 0.4920 \\ 1.0706 \\ -1.3265 \\ 1.5101$	-1.2403 -0.0670 -0.2254 1.8399 -0.9027	0.003 0.003 0.003 0.003 0.003	

Table 4. Values of the Coefficients B_i of Eq 2 and the Standard Deviations, $\delta(n_D)$, for the Various Mixtures at 303.15 K

mixture	B_1	B_2	B_3	B_4	$\delta(n_{\rm D})$
$xn-C_7H_{15}OH + (1 - x)n-C_5H_{12}$	1.351 84	0.071 21	-0.007 32	0.004 63	0.0002
$xn-C_7H_{15}OH + (1 - x)n-C_6H_{14}$	1.369 49	0.048 96	0.005 65	-0.00401	0.0002
$xn-C_7H_{15}OH + (1 - x)n-C_7H_{16}$	1.382 34	0.037 79	0.001 61	$-0.001\ 61$	0.0002
$xn-C_7H_{15}OH + (1 - x)n-C_8H_{18}$	1.392 52	0.025 35	0.005 47	-0.00328	0.0002
$xn-C_7H_{15}OH + (1 - x)2,2,4-TMP$	1.386 42	0.035 46	-0.004 87	0.003 33	0.0001

pointed out by Berro and Péneloux (1984), the calculations were performed for all these systems with D = 25. The values of the coefficients A_j of eq 1, along with the standard deviations, $\delta(V_{\rm m}^{\rm E})$, for the various mixtures are given in Table 3.

The refractive indexes, n_D , of the present mixtures at 303.15 K have been fitted by the method of least squares to the equation

$$n_{\rm D} = \sum_{j=1}^{m} B_j x^{j-1}$$
 (2)

The values of the coefficients B_j of eq 2, along with the standard deviations, $\delta(n_D)$, are given in Table 4.

 $V_{\rm m}^{\rm E}$ is positive at lower mole fractions of *n*-C₇H₁₅OH for *xn*-C₇H₁₅OH + (1 - *x*)*n*-C₇H₁₆, *xn*-C₇H₁₅OH + (1 - *x*)*n*-C₈H₁₈, and *xn*-C₇H₁₅OH + (1 - *x*)2,2,4-TMP and is negative at higher mole fractions of *n*-C₇H₁₅OH for these mixtures, with inversion of sign of $V_{\rm m}^{\rm E}$ from positive to negative values occurring at $x \sim 0.20$, $x \sim 0.45$, and $x \sim 0.06$, respectively, for the above mixtures at T = 308.15 K. $V_{\rm m}^{\rm E}$ is found to be negative throughout the entire range of composition for *xn*-C₇H₁₅OH + (1 - *x*)*n*-C₅H₁₂ at T = 298.15 K, and for *xn*-C₇H₁₅OH + (1 - *x*)*n*-C₆H₁₄ at T = 308.15 K. At x = 0.5, $V_{\rm m}^{\rm E}$ for the various present mixtures of *n*-C₇H₁₅OH with alkanes has the sequence

$$n-C_8H_{18} > n-C_7H_{16} > 2,2,4-TMP > n-C_6H_{14} > n-C_5H_{12}$$

It is quite interesting to note that the above (same) sequence is also found (Nath and Pandey, 1997) in the values of V_m^E at x = 0.5, and at T = 298.15 K, for binary mixtures of butanol (n-C₄H₉OH) with n-C₅H₁₂, n-C₆H₁₄, n-C₇H₁₆, n-C₈H₁₈, and 2,2,4-TMP.

The values of $V_{\rm m}^{\rm E}$ of the (alkanol + alkane) mixtures may be interpreted as the result of the contributions of the various types of intermolecular interactions operating between the alkane and alkanol molecules. Mainly three type of the contributions, (i) physical, due to nonspecific interactions; (ii) chemical, due to hydrogen bonding, and (iii) structural, due to changes of interstitial accommodation and free volume, are important in determining the thermodynamic excess properties of the alkanol + alkane mixtures. The chemical contribution is important at low concentrations of alkanol, where the breaking of selfassociation of the alkanol molecules due to H bonds makes a positive contribution to V_m^E . The positive values of V_m^E for xn-C₇H₁₅OH + (1 - x)n-C₇H₁₆, xn-C₇H₁₅OH + (1 - x) $n-C_8H_{18}$, and $xn-C_7H_{15}OH + (1 - x)^2 + 2x^2 + 1$ at low x values may thus be attributed to the predominance of the contributions to the values of V_m^E due to the breaking of self-association due to H bonds in the heptanol molecules in these mixtures.

Literature Cited

- Berro, C.; Péneloux, A. Excess Gibbs Energies and Excess Volumes of 1-Butanol-n-Heptane and 2-Methyl-1-propanol-n-Heptane Binary Systems. J. Chem. Eng. Data 1984, 29, 206–210.
- $\begin{array}{l} Franjo, C.; Lorenzana, M. T.; Legido, J. L.; Andrade, M. I. P.; Jiménez, E. Excess Molar Volumes of [x_1CH_3CH_2CO_2(CH_2)_2CH_3 + x_2CH_3(CH_2)_5-OH + (1 x_1 x_2) \{CH_3(CH_2)_4CH_3 \mbox{ or } c-C_6H_{12}\}] at the temperature 298.15 K. J. Chem. Thermodyn.$ **1994**,*26* $, 1025–1030. \end{array}$
- Fuente, I. G. D.; Rodríguez, J. F.; González, J. A.; Cobos, J. C.; Casanova, C. Excess Molar Volumes of (n-Nonan-1-ol + n-Decane or n-Tetradecane) at the temperatures of 298.15 K, 308.15 K, and 318.15 K. J. Chem. Thermodyn. 1992, 24, 23–27.
- Heintz, A.; Schmittecker, B.; Wagner, D.; Lichtenthaler, R. N. Excess Volumes of 1-Alkanol/Hexane Mixtures at Temperatures between 283.15 and 323.15 K. J. Chem. Eng. Data 1986, 31, 487–492.
- Nath, J.; Saini, R. Excess Volumes for Binary Liquid Mixtures of Methylethylketone with Methylene Chloride, 1,2-Dichloroethane, Trichloroethylene, Tetrachloroethylene and Cyclohexane at Various Temperatures. *Fluid Phase Equilib.* **1989**, *50*, 297–303.
- Nath, J.; Chaudhary, S. K. Excess Volumes, Dielectric Constants, Refractive Indexes, and Viscosities for Anisole + Methylene Chloride, 1,2-Dichloroethane, Trichloroethene, Tetrachloroethene and Cyclohexane. J. Chem. Eng. Data **1992**, *37*, 387–390.
- Nath, J.; Pandey, J. G. Binary Mixtures of Butanol + Pentane, + Hexane, + Heptane, + Octane, + 2,2,4-Trimethylpentane, and + Carbon tetrachloride. 1. Excess Molar Volumes at 288.15 K and 298.15 K and Refractive Indexes at 298.15 K. J. Chem. Eng. Data 1997, 42, 128–131.
- Riddick, J. A.; Bunger, W. B. Organic Solvents: Physical Properties and Methods of Purification, 3rd ed.; Techniques of Chemistry, Vol. II; Wiley: New York, 1970.
- Wagner, D.; Heintz, A. Excess Volumes of Binary 1-Alkanol/Nonane Mixtures at Temperatures between 293.15 and 333.15 K. J. Chem. Eng. Data 1986, 31, 483–487.
- Zielkiewicz, J. (Vapour + Liquid) Equilibria in (Heptane + Propan-2-ol or Butan-1-ol or 2-Methylpropan-1-ol or 2-Methylpropan-2-ol or Pentan-1-ol) at the Temperature 313.15 K. *J. Chem. Thermodyn.* **1994a**, *26*, 919–923.
- Zielkiewicz, J. Excess Volumes of (Heptane + Propan-2-ol or Butan-1-ol or 2-Methylpropan-1-ol or 2-Methylpropan-2-ol or Pentan-1-ol) at the Temperature 313.15 K. J. Chem. Thermodyn. 1994b, 26, 959–964.

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